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## COMPLETE LISTING OF CLAIMS, INCORPORATING AMENDMENTS IN RESPONSE TO OFFICE ACTION DATED 3/9/2004 AND TELEPHONE INTERVIEW DATED 5/10/2004 FOR SERIAL NO. 09/759,781

Claim 1. (withdrawn)

An apparatus for extracting and sequestering CO2 from a

gas stream, comprising:

a reactor vessel;

an aqueous solution;

means for introducing said gas stream into said reactor vessel;

carbonate disposed in said reactor vessel, wherein said carbonate is of the form  $X(CO_3)_m$  wherein X is any element or combination of elements that can chemically bond with a carbonate group or its multiple, wherein at least one said element is a group IA, IIA, IIIA, IVA, IB, IIB, IIIB, IVB, VB, VIB, VIIB, or VIIIB element of the periodic table, and wherein m is a stoichiometrically determined positive integer;

means for hydrating said CO<sub>2</sub> with said aqueous solution to form carbonic acid, thereby resulting in a CO<sub>2</sub>-depleted gas stream;

means for removing said CO<sub>2</sub>-depleted gas stream from said reactor vessel; means for reacting said carbonate with said carbonic acid to form a waste stream solution of metal ions and bicarbonate;

means for removing said waste stream solution from said reactor vessel; a disposal site:

means for pre-treating said waste stream solution to reduce the amount of CO<sub>2</sub> outgassing and carbonate precipitation that may occur after said waste stream solution is released into said disposal site; and

means for releasing said pretreated waste stream solution into said disposal site.

Claim 2. (withdrawn) The apparatus as recited in claim 1 wherein:
said pre-treating means comprises CO<sub>2</sub> degassing means selected from the group
consisting of means for allowing said waste stream solution to degas CO<sub>2</sub> to an

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overlying headspace whose pCO<sub>2</sub> is less than that of said waste stream solution; means for purging said waste stream with a gas stream whose pCO<sub>2</sub> is less than that of the waste stream; and means for applying a partial vacuum to the headspace above the waste stream.

- Claim 3. (withdrawn) The apparatus as recited in claim 1 wherein: said pre-treating means comprises means for diluting said waste stream solution with a second solution that is undersaturated with respect to CO<sub>2</sub>, carbonate ions or both CO<sub>2</sub> and carbonate ions.
- Claim 4. (withdrawn) The apparatus as recited in claim 1 wherein: said pre-treating means comprises means for adding chemical additives which impede carbonate precipitation, said chemical additives being selected from the group consisting of phosphate, metals, and organic compounds, said organic compounds being selected from the group consisting of EDTA, humic substances, aromatic acids, citrate, malate, pyruvate, glycelglycerine, glycogen, arginine, glutamate, glycine, glycoprotein succinate, taurine, chondroitin sulfate, galactose, dextrose and acetate.
- Claim 5. (withdrawn) The apparatus as recited in claim 1 wherein: said pre-treating means comprises ion exchange means for exchanging at least a portion of the Ca<sup>2+</sup> cations present in said waste solution with exchange cations which when balanced by the CO<sub>3</sub><sup>2-</sup> anions present in the waste solution exhibit greater solubility and less propensity for precipitation than does CaCO<sub>3</sub>.
- Claim 6. (withdrawn) The apparatus as recited in claim 5 wherein:
  said ion exchange means comprises passing said waste stream solution through an
  ion exchange column, with said column containing Na<sup>+</sup> exchange ions.
- Claim 7. (withdrawn) The apparatus as recited in claim 1 wherein: said pre-treating means comprises ion exchange means for exchanging at least a

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portion of the CO<sub>3</sub><sup>2</sup> anions present in said waste solution with other anions.

- Claim 8. (withdrawn) The apparatus as recited in claim 7 wherein:
  said ion exchange means comprises passing said waste solution through an ion
  exchange column containing Cl anions.
- Claim 9. (withdrawn) The apparatus as recited in claim 1 wherein:

  said pre-treating means comprises means for increasing the density of said waste stream solution.
- Claim 10. (withdrawn) The apparatus as recited in claim 1 wherein: said disposal site comprises a large body of water that is either freshwater or seawater.
- Claim 11. (withdrawn) The apparatus as recited in claim 10 wherein:
  the pCO2 of said body of water at the point of release of waste stream solution is
  less than that of said waste stream solution.
- Claim 12. (withdrawn) The apparatus as recited in claim 10 wherein: said releasing means comprises means for releasing said waste stream solution at a depth sufficient for mixing and dilution of said waste stream solution with said body of water to occur.
- Claim 13. (withdrawn) The apparatus as recited in claim 10 wherein:
  said releasing means comprises means for releasing said waste stream solution at a
  depth wherein the pressure and temperature existent at said depth is sufficient to
  impede CO<sub>2</sub> outgassing to the atmosphere and carbonate precipitation.
- Claim 14. (withdrawn) The apparatus as recited in claim 10 wherein:
  said large body of water is either a sea or ocean; and
  said releasing means causes said waste stream solution to be released below the

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pycnocline.

- Claim 15. (withdrawn) The apparatus as recited in claim 10 wherein:
  said large body of water is either a sea or ocean; and
  said releasing means causes said waste stream solution to be released in the vicinity
  of a reef, above the pycnocline.
- Claim 16. (withdrawn) The apparatus as recited in claim 10 wherein: said disposal site is a body of surface seawater having sufficient constituents that serve to impede carbonate precipitation, said constituents being phosphate, Mg<sup>2+</sup> ions, or phosphate and Mg<sup>2+</sup> ions.
- Claim 17. (withdrawn) The apparatus as recited in claim 10 wherein: said disposal site is a large body of surface seawater having sufficient organic compounds that serve to at least partially impede carbonate precipitation, said organic compounds selected from the group consisting of humic substances, aromatic acids, citrate, malate, pyruvate, glycelglycerine, glycogen, arginine, glutamate, glycine, glycoprotein succinate, taurine, chondroitin sulfate, galactose, dextrose and acetate.
- Claim 18. (Currently Amended) A method of extracting and sequestering CO<sub>2</sub> from a gas stream, said method comprising the steps of:

  hydrating said CO<sub>2</sub> in said gas stream with an aqueous solution to form carbonic acid, thereby resulting in a CO<sub>2</sub>-depleted gas stream;

  reacting said carbonic acid with carbonate to form a waste stream solution of metal ions and bicarbonate, wherein said carbonate is of the form X(CO<sub>3</sub>)<sub>m</sub> wherein X is any element or combination of elements that can chemically bond with a carbonate group or its multiple, wherein at least one said element is a group IA, IIA, IIIA, IVA, IB, IIB, IIIB, IVB, VB, VIB, VIIB, or VIIIB element of the periodic table, and wherein m is a stoichiometrically determined positive integer;

  pre-treating said waste stream solution to reduce the amount of CO<sub>2</sub> outgassing and

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carbonate precipitation that may occur after said waste stream solution is released into a disposal site; and releasing said pre-treated waste stream solution into said disposal site, wherein said disposal site comprises a large body of water.

- Claim 19. (original) The method as recited in claim 18 wherein:
  said pre-treating step comprises a CO<sub>2</sub> degassing step selected from the group
  consisting of allowing said waste stream solution to degas CO<sub>2</sub> to an overlying
  headspace whose pCO<sub>2</sub> is less than that of said waste stream solution; purging said
  waste stream with a gas stream whose pCO<sub>2</sub> is less than that of the waste stream;
  and applying a partial vacuum to the headspace above the waste stream.
- Claim 20. (Previously Presented) The method as recited in claim 18 wherein: said pre-treating step comprises diluting said waste stream solution with a second solution that is undersaturated with respect to CO<sub>2</sub>, carbonate ions, or both CO<sub>2</sub> and carbonate ions.
- Claim 21. (Previously Presented) The method as recited in claim 18 wherein: said pre-treating step comprises adding chemical additives which impede carbonate precipitation, said chemical additives being selected from the group consisting of phosphate, metals, and organic compounds, said organic compounds being selected from the group consisting of EDTA, humic substances, aromatic acids, citrate, malate, pyruvate, glycelglycerine, glycogen, arginine, glutamate, glycine, glycoprotein succinate, taurine, chondroitin sulfate, galactose, dextrose and acetate.
- Claim 22. (original) The method as recited in claim 18 wherein:
  said pre-treating step comprises exchanging at least a portion of the Ca<sup>2+</sup> cations
  present in said waste solution with exchange cations which when balanced by the
  CO<sub>3</sub><sup>2-</sup> anions exhibit greater solubility and less propensity for precipitation than
  does CaCO<sub>3</sub>.

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- Claim 23. (original) The method as recited in claim 22 wherein:
  said cation exchanging step comprises passing said waste stream solution through
  an ion exchange column, with said column containing Na<sup>+</sup> exchange ions.
- Claim 24. (Previously Presented) The method as recited in claim 18 wherein: said pre-treating step comprises exchanging at least a portion of the CO<sub>3</sub><sup>2-</sup> anions present in said waste solution with other anions.
- Claim 25. (Previously Presented) The method as recited in claim 24 wherein: said anion exchanging step comprises passing said waste solution through an ion exchange column containing Cl anions.
- Claim 26. (original) The method as recited in claim 18 wherein: said pre-treating step comprises increasing the density of said waste stream solution.
- Claim 27. (Previously Presented) The method as recited in claim 18 wherein: said disposal site comprises a large body of water that is either freshwater or seawater.
- Claim 28. (original) The method as recited in claim 27 wherein: the pCO<sub>2</sub> of said body of water at the point of release of waste stream solution is less than that of said waste stream solution.
- Claim 29. (original) The method as recited in claim 27 wherein:
  said releasing step comprises releasing said waste stream solution at a depth
  sufficient for mixing of said waste stream solution with said body of water to occur.
- Claim 30. (original) The method as recited in claim 27 wherein:

  said releasing step comprises releasing said waste stream solution at a depth

  wherein the pressure and temperature existent at said depth is sufficient to impede

  CO<sub>2</sub> outgassing to the atmosphere and carbonate precipitation.

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- Claim 31. (original) The method as recited in claim 27 wherein:

  said large body of water is either a sea or ocean; and

  said releasing step comprises releasing said waste stream solution below the

  pycnocline.
- Claim 32. (original) The method as recited in claim 27 wherein:
  said large body of water is either a sea or ocean; and
  said releasing step comprises releasing said waste stream solution in the vicinity of
  a reef, above the pycnocline.
- Claim 33. (original) The method as recited in claim 27 wherein: said disposal site is a body of surface seawater having sufficient constituents that serve to impede carbonate precipitation, said constituents being phosphate, Mg<sup>2+</sup> ions, or phosphate and Mg<sup>2+</sup> ions.
- Claim 34. (original) The method as recited in claim 27 wherein:
  said disposal site is a body of surface seawater having sufficient organic compounds
  that serve to impede carbonate precipitation, said organic compounds selected from
  the group consisting of humic substances, aromatic acids, citrate, malate, pyruvate,
  glycelglycerine, glycogen, arginine, glutamate, glycine, glycoprotein succinate,
  taurine, chondroitin sulfate, galactose, dextrose and acetate.
- Claim 35 (Previously Presented) The method as recited in claim 27 wherein:
  said large body of water is either a sea or ocean; and
  said releasing step comprises releasing said waste stream solution at a depth below
  the carbonate compensation depth (CCD).